

Mechanisms of chemical kinetics: detailed modelling and model reduction

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Outline

- Introduction
 - mechanisms of chemical kinetics of combustion
- Problem statement of model reduction
 - dimensionality, non-linearity, stiffness
- Methodology
 - empirical standard / conventional methods
 - Iocal and global multiple time-scales analysis
 - system degeneration, time scale separation, Global Quasi-Linearization (GQL)
- Implementation example
 - Auto-ignition problem of hydrogen/oxygen combustion system
- Summary, acknowledgments and future work

Problem Statement: $2H_2+O_2 = 2H_2O_2$



- Modelling of combustion wave, p = const
- Mass balance $\rho_{\infty} v_{\infty} = \rho_0 v_0$
- Energy balance $h_{\infty} = h_0$
- Calculation of the temperature:

$$h_{\text{H}_{2}\text{O}}(T_{\infty}) = h_{\infty} = h_{0} = w_{\text{H}_{2}}h_{\text{H}_{2}}(T_{0}) + w_{\text{O}_{2}}h_{\text{O}_{2}}(T_{0})$$

- Problem: Model: T = 4800 K, only H₂O present in Products
 Reality: T = 3090 K, H₂O, O₂, H₂, OH, H, O in Products
- Meaning: no information how chemical reaction occurs no information on the composition of the mixture
- What to do in order to improve this situation?

Radicals chain reactions of H_2-O_2 - combustion system $\bullet H_2 + O_2 = OH + OH$ chain initiation $\bullet OH + H_2 = H_2O + H$ chain branching •H + O_2 = OH + O chain branching $\bullet O + H_2 = OH + H$ chain branching •H = $1/2 H_2$ chain termination (e.g. on the wall) $-H + O_2 + M = HO_2 + M$ chain termination (homogenous) For T < 1100 K additional channel has to be accounted for!</p>

 $\begin{array}{rcl} \bullet HO_2 & + H_2 & = & H_2O_2 & + & H \\ \bullet H_2O_2 & + & M & = & OH + OH + M \end{array}$

Mechanisms of detailed chemical kinetics -Example



H_2 / O_2	Mechanism
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	O ₂	+ H	<u>= OH</u>	+ O	
<	H_2	+ O	= OH	+ H	
	H_2	+ OH	$= H_2O$	+ H	
	OH	+ OH	$= H_2O$	+ O	
	Н	+ H + M	$= H_2$	+ M	
	Н	+ OH + M	$= H_2O$	+ M	
	0	+ O + M	= O ₂	+ M	
	Н	+ O ₂ + M	$= HO_2$	+ M	
	HO_2	+ H	= OH	+ OH	
	HO ₂	+ H	$= H_2$	+ O ₂	d
	HO_2	+ H	$= H_2O$	+ O	_
	HO ₂	+ O	= OH	+ O ₂	
	HO_2	+ OH	$= H_2O$	+ O ₂	đ
	HO_2	+ HO ₂	$= H_2O_2$	+ O ₂	
	OH	+ OH + M	$= H_2O_2$	+ M	
	H_2O_2	+ H	$= H_2$	+ HO ₂	
	H_2O_2	+ H	$= H_2O$	+ OH	
	H_2O_2	+ O	= OH	+ HO ₂	
	H_2O_2	+ OH	$= H_2O$	+ HO ₂	

see e.g.: Warnatz, Maas, Dibble: Combustion, Springer 2004

 Hydrogen/air combustion mechanism consists of 19 elementary reactions

 $(n_r = 19)$ between 9 species $(n_s = 9)$

 Even for simplest possible combustion system the dimension is quite high

$$\frac{d[H_{2}]}{dt} = -R_{2} - R_{3} + R_{5} + \dots$$

$$R_{2}(\psi) = A_{2}^{+}e^{-\frac{E_{2}^{+}}{RT}}[H_{2}][O] - A_{2}^{-}e^{-\frac{E_{2}^{-}}{RT}}[OH][H]$$

$$\frac{d[H_{2}O_{2}]}{dt} = R_{15} + R_{16} - \dots$$

$$\frac{d\psi}{dt} = \begin{pmatrix} S_{1,1} & S_{1,2} & \dots & S_{1,n_{r}} \\ \dots & \dots & \dots & \dots \\ S_{n_{s},1} & S_{n_{s},2} & \dots & S_{n_{s},n_{r}} \end{pmatrix} \cdot \begin{pmatrix} R_{1}(\psi) \\ R_{2}(\psi) \\ \dots \\ R_{n_{r}}(\psi) \end{pmatrix} = \begin{pmatrix} F_{1}(\psi) \\ F_{2}(\psi) \\ \dots \\ F_{n}(\psi) \end{pmatrix}$$
er 2004

Predictions of the thermodynamics of the chemical kinetics



- Composition of the products:
- H₂-O₂ combustion system
- T_∞ = 3080 K, 57 % H₂O, 5 % O₂,16 % H₂, 10 % OH, 8 % H, 4 % O



Ref.: Warnatz, Maas, Dibble: Combustion

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Mechanisms of detailed chemical kinetics - dimenisonality

 Overall dimension of a reacting system is defined by a number of species minus number of conserved quantities

$$n_s \sim O(100), \quad n_r \sim O(1000)$$

Do we really need so many parameters to describe the process with prescribed accuracy?

complete, ver 10 C14 (LLNL) Number of reactions, n-heptane (LLNL) 10³ before 2000 2000-2004 2005-2009 10² since 2010 = 5K 10² 10³ 10⁴ 10

Ranzi mechanism

Number of species, K

Ref.: F.N. Egolfopoulos, N. Hansen, Y. Ju, K. Kohse-Höinghaus, C.K. Law, F. Qi
 Advances and challenges in laminar flame experiments and implications for combustion chemistry,
 Progress in Energy and Combustion Science, Volume 43, August 2014, Pages 36-67.



2-methyl alkanes (LL

methyl palmitate (CNR

Mechanisms of detailed chemical kinetics -Stiffness





1-dimensional cut through a CH_4 -air flame (n_s=33)

- Non-linear chemical source term leads to stiffness of the governing
 equations system
- ^{1,0 10⁻⁷} Furthermore, different chemical time scales do not only introduce stiffness, but also cause the existence of very small length scales

Mechanisms of detailed chemical kinetics



- Brief overview
 - "too many" species are involved in accurate modeling of combustion process participating in
 - several thousand elementary reactions with a little known about their rates

leading to

- stiffness of system of governing equations and
- high dimensionality of thermo-kinetic state of combustion system

Solution I: skeletal mechanisms



- The model is reduced by removing (neglecting) particular elementary reactions or species
 - If a specific set of system parameters and conditions is considered, then
 - Hydrogen, Syngas ~10
 - Methane ~30
 - Heptane ~50
 - etc.

Binomial[300,30] =173193226149263513034110205899732811401360= 1.73193×10⁴¹

• More sophisticated methodologies have to be developed to proceed beyond these limits!

Solution II: standard approaches – QSSA



The decomposition can be represented by species

$$\frac{d\psi}{dt} = \begin{pmatrix} s_{1,1} & s_{1,2} & \dots & s_{1,n_r} \\ \dots & \dots & \dots & \dots \\ s_{n_s,1} & s_{n_s,2} & \dots & s_{n_s,n_r} \end{pmatrix} \cdot \begin{pmatrix} R_1(\psi) \\ R_2(\psi) \\ \dots \\ R_n(\psi) \end{pmatrix} = \begin{pmatrix} F_1(\psi) \\ F_2(\psi) \\ \dots \\ F_n(\psi) \end{pmatrix}$$

Some species are assumed to be at quasi-steady states (QSS)

$$M_{QSSA}^{0} = \left\{ F_{j_{1}}(\psi) = 0, \dots, F_{j_{n-m}}(\psi) = 0 \right\}$$

$$M_{QSSA}^{0, fast} = \left\{ \psi_{j_{1}} = const, \dots, \psi_{j_{n-m}} = const \right\}$$

$$\frac{d[H_{2}]}{dt}$$

$$\dots$$

$$\frac{d[H_{2}]}{dt}$$

$$\frac{d[H_2]}{dt} = F_1(\psi) = -R_2 - R_3 + R_5 + \dots$$

$$\frac{d[H_2O_2]}{dt} = F_{n_s}(\psi) = R_{15} + R_{16} - \dots$$

• The choice of the species $\{j_1, \ldots, j_{n-m}\}$ is very crucial

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Solution II: standard approaches – PEA

 $M_{PEA}^{0} = \left\{ R_{i_{1}}(\psi) = 0, ..., R_{i_{n_{f}}}(\psi) = 0 \right\} \quad m = n - n_{f}$

The decomposition can be represented by using elementary reaction rates

$$\frac{d\psi}{dt} = F(\psi) = \begin{pmatrix} s_{1,1} & s_{1,2} & \dots & s_{1,n_r} \\ \dots & \dots & \dots & \dots \\ s_{n_s,1} & s_{n_s,2} & \dots & s_{n_s,n_r} \end{pmatrix} \begin{pmatrix} R_1(\psi) \\ R_2(\psi) \\ \dots \\ R_n(\psi) \end{pmatrix} = \begin{pmatrix} F_1(\psi) \\ F_2(\psi) \\ \dots \\ F_n(\psi) \end{pmatrix}$$

Some elementary reactions are assumed to be at partial equilibrium

$$\frac{d[H_2]}{dt} = F_1(\psi) = -R_2 - R_3 + R_5 + \dots$$

...
$$\frac{d[H_2O_2]}{dt} = F_{n_s}(\psi) = R_{15} + R_{16} - \dots$$

• The choice of the elementary reactions $\{i_1, \dots, i_{n-m}\}$ becomes crucial

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Solutions I+II: standard approaches – Problems



 Original coordinates of the system might not be suitable for the decomposition in terms of the species or elementary reactions

 Approximation of the system solution by either QSSA or PEA might be valid in a narrow range of the system parameters

 Empirical choice of such reactions and/or species is very demanding!

Concept: dimension reduction

- Problems of detailed chemical kinetics:
 - several hundreds chemical species
 - several thousands elementary reactions
 - stiffness of the governing equations system
- But: only few reactions are rate limiting!
- Fundamental concepts:
 - Multiple time scales
 - Decomposition of motions
 - Existence of manifolds of fast and slow motions



Solution III: Multiple time scales – ILDM, GQL



• Reactions and combination of species are identified corresponding to relevant characteristic time scales $\tau_i = 1/|\lambda_i|$

$$\frac{d\psi}{dt} = F(\psi) = \begin{pmatrix} s_{1,1} & s_{1,2} & \dots & s_{1,n_r} \\ \dots & \dots & \dots & \dots \\ s_{n_s,1} & s_{n_s,2} & \dots & s_{n_s,n_r} \end{pmatrix} \cdot \begin{pmatrix} R_1(\psi) \\ R_2(\psi) \\ \dots \\ R_n(\psi) \end{pmatrix} = \begin{pmatrix} F_1(\psi) \\ F_2(\psi) \\ \dots \\ F_n(\psi) \end{pmatrix} = \begin{bmatrix} Z_1 Z_2 \dots Z_n \end{bmatrix} \begin{bmatrix} \lambda_1 & 0 & \dots & 0 \\ 0 & \lambda_2 & \dots & 0 \\ \dots & \dots & \dots & \dots \\ 0 & 0 & \dots & \lambda_n \end{bmatrix} \begin{bmatrix} \tilde{Z}_1 \\ \tilde{Z}_2 \\ \dots \\ \tilde{Z}_n \end{bmatrix}$$

 Thus, manifold (states) accounting for partially equilibrating processes described by invariant eigenspaces becomes available:

$$M_{ILDM} = \left\{ \widetilde{Z}_{I}^{f}(\psi) \cdot F(\psi) = 0, ..., \widetilde{Z}_{I}^{f}(\psi) \cdot F(\psi) = 0 \right\}$$

- The problem of the empirical choice is overcome!
 - Ref.: Maas, Pope, Comb. Flame (1992)

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Solution III: ILDM application – Syngas

- Syngas mechanism n_r =38, n_s=13 is considered
- 2D, 3D manifolds of relatively slow motion are calculated and tabulated
- A number of detailed system solution trajectories are shown



 Tabulation concept permits efficient application $CO-H_2-O_2$ homogeneous system, magenta – system trajectories, blue is 2D ILDM, green represents 3D ILDM





Solution III: Overview

- Rigorous time scale analysis allows us
 - Check the system hierarchy!
 - Estimate the reduced dimension!
 - Approximate manifolds representing reduced model!
 - Decompose the system!

 Ref.: Bykov, Gol'dshtein, Maas, CTM, 12(2), 389 – 405 (2008)



 $CO-H_2-O_2$ homogeneous system, red line – system trajectory, blue mesh is 2D ILDM mesh, green line represents (n-m)dim. fast relaxation part of the trajectory

ILDM versus GQL



The system dynamics can be decomposed explicitly



• Ref.: Bykov, Gol'dshtein, Maas, CTM, 12(2), 389 - 405 (2008)



Application of the standard method - QSSA



QSSA for different species under

 $p_0 = 1 \text{ bar and } \Phi = 1.0 \text{ for } 900 \text{ } K \le T_0 \le 2000 \text{ } K.$



Comparison of the GQL and the best performing QSSA



• The ignition delay time at $p_0 = 1 \ bar$ and $\Phi = 1.0$. On the left: delay time prediction, right figure: relative errors in % versus initial temperature T_0 .



Comparison of the GQL and the best performing QSSA



• The ignition delay time at $T_0 = 1200 K$ and $\Phi = 1.0$. Left figure: delay times; right figure: relative errors in % versus initial pressure p_0 .



Comparison of the GQL and the best performing QSSA



• The ignition delay time at $T_0 = 1200 K$ and $p_0 = 1 bar$. Left figure: delay times; right figure: relative errors in % versus initial fuel/air equivalence ratio Φ .



Comparison of the GQL and the best performing QSSA, time history



• Time history of species H₂ (a), OH (b), HO₂ (c) and H₂O (d) Specific mole number is given in $\phi_i = [w_i/M_i] = mol/g$

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Summary

- The problem of detailed modelling of combustion kinetics was discussed
- Methods to treat and implement model reduction of combustion systems were outlined
- Key concepts of multiple time scales, decomposition of motions as well as a transparent application example was presented

Acknowledgments: Ulrich, Vladimir, Chunkan Yu...

Future work, questions



One has to use the multiple-time scale separation explicitly!



Thank you very much for your attention!

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Network of chemical (elementary) reactions:

Elementary reaction rates:

Model

$$R_{1}(\psi) = k_{1}^{+}(T)[A][M] - k_{1}^{+}(T)[A][A^{*}]$$

$$R_{2}(\psi) = k_{2}^{+}(T)[A^{*}], \quad \psi = ([A], [A^{*}], [P])$$

Dynamical system as a system of ODEs:

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Mechanisms of detailed chemical kinetics -Modelling

example - Lindemann mechanism:
$$A \rightarrow P$$

$$k_1 : A + M \quad \leftrightarrow \quad A^* + M$$
$$k_2 : A^* \to P$$

$$M = \alpha_{A}A + \alpha_{B}A^{*} + \alpha_{P}P$$

$$\frac{d[A]}{dt} = -R_1 = -k_1^+(T)[A][M] + k_1^+(T)[A][A^*]$$
$$\frac{d[A^*]}{dt} = R_1 - R_2 \implies \psi = (A, A^*)$$
$$\frac{d[P]}{dt} = R_2 \implies [A] + [A^*] + [P] = [A]_0$$



Mechanisms of detailed chemical kinetics – Dynamical system



$$\psi = \left(\begin{bmatrix} A \end{bmatrix} / \begin{bmatrix} A \end{bmatrix}_{0}, \begin{bmatrix} A^{*} \end{bmatrix} / \begin{bmatrix} A \end{bmatrix}_{0} \right)$$

$$\frac{d\psi_{1}}{dt} = -R_{1}(\psi_{1}, \psi_{2}), \quad \psi_{1}(t=0) = 1$$

$$\frac{d\psi_{2}}{dt} = R_{1}(\psi_{1}, \psi_{2}) - R_{2}(\psi_{1}, \psi_{2}), \quad \psi_{2}(t=0) = 0$$

$$d\tau$$

$$R_1(\psi) = \psi_1^2 - K_1 \psi_1 \psi_2$$
$$R_2(\psi) = K_2 \psi_2$$

 $=k_{1}^{+}[A]_{0}dt$

Dimensionless form of the system with stoichiometric matrix and reaction rate vector

$$\frac{d}{d\tau} \begin{pmatrix} \psi_1 \\ \psi_2 \end{pmatrix} = \begin{pmatrix} -1 & 0 \\ 1 & -1 \end{pmatrix} \begin{pmatrix} R_1(\psi_1, \psi_2) \\ R_2(\psi_1, \psi_2) \end{pmatrix} \Rightarrow \frac{d\psi}{d\tau} = F(\psi)$$

Two model parameters controlling elementary reaction rates

$$K_1 = \frac{k_1^-}{k_1^+}, \quad K_2 = \frac{k_2^+}{k_1^+ [A]_0}$$

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Mechanisms of detailed chemical kinetics -Properties

 Smooth dependence on system parameters (rate constants)

$$\frac{d}{dt}\begin{pmatrix}\psi_1\\\psi_2\end{pmatrix} = \begin{pmatrix}-1 & 0\\1 & -1\end{pmatrix}\begin{pmatrix}R_1(\psi_1,\psi_2)\\R_2(\psi_1,\psi_2)\end{pmatrix}$$

 Typically system solution has particular properties: relatively fast transient following smooth evolution towards global equilibrium

$$K_1 = 1, \quad K_2 = 0.1$$





Solution III: ILDM application – Lindemann mechanism

ILDM, PEA and QSSA are compared

Decomposition is identified automatically and independently on particular choice

Thus, the main problem of the empirical choice is overcome!



1.0 0.8 0.6 Ψ_2 0.4 0.2 0.0 0.0 0.2 0.4 0.6 0.8 1.0 ψ_1

Green line is PEA curve, red line represents

QSSA, while red line represents ILDM curve





Rigorous time scale analysis allows us



 State space projection into O-H-OH space with trajectories calculated based on detailed kinetics model (coloured lines). Green points are the candidate selected points.